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## METHOD OF MAKING OPTICAL FIBRES

### Background of the Invention

#### 5 Field of the Invention

The present invention relates to the manufacture of optical fibres. In particular, the invention concerns a method according to the preamble of claim 1 of subjecting a glass preform to processing by tensile forces in a heating oven for making of optical fibres or for stretching of the glass perform into a form suitable for fibre manufacture. The present invention is also concerned with an apparatus according to the preamble of claim 17 for processing of glass preforms.

#### 15 Description of Related Art

In the manufacture of optical fibres, a glass preform, comprising, for example, a layered glass structure, is drawn through a furnace having a jacket defining an elongated heating chamber, with a vertically or horizontally oriented central axis, in which the preform is heated to temperatures in the range of about 1800 to 2200 °C in order to soften the glass. In practice, furnaces having either ZrO or graphite resistances (resistance heating or induction heating) are used. In both cases, at the inlet opening, through which the, for example, vertically suspended glass preform extends into the oven, a seal is provided. The seal can comprise a mechanical ring, such as a mechanical iris structure, which will reduce the clearing between the inlet orifice and the exterior walls of the preform.

25 With furnaces having ZrO resistances, the processing can be carried out in ambient atmosphere and the sealing efficiency of the inlet orifice is not critical. Nor is there any particular need for minimizing the clearing between the glass preform and the inner surface of the inlet opening. However, these furnaces are hampered by the considerable disadvantage that the constructions are destroyed, if they are allowed to cool down during operation. Thus, particularly difficult situations may arise during power failures and similar malfunctions.

35 The second heating oven, viz. the graphite furnace, is used more extensively. In order to avoid burning the graphite, the graphite parts of the furnace should be kept in a protective atmosphere at temperatures over 500 °C. It can be noted that not only is it expensive to renew the graphite resistances, which have been burnt, but glowing and smoking graphite also causes formation of particles that weakens the properties of the fibre.

Therefore, in case of graphite furnaces, an essential part in controlling the protective atmosphere is the provision of an efficient sealing 1) between the glass preform, which is fed into the furnace, 2) inside the furnace, and 3) between the drawn fibre/preform and the outlet of the furnace body, respectively. So far, there has been no proper way of controlling these seals.

Various mechanical seals are disclosed in JP Published Patent Application No. 55 020260, US Patent No. 4,477,274, DE Patents Nos. 3 903 466 and 4 006 839, wherein dragging elastomer or graphite seals are described. These seals fit snugly against the preform during drawing of the fibre.

A typical mechanical sealing of the kind mentioned above is also shown in the attached Figure 2. In the figure, reference numeral 1 stands for the supporting block of the iris, 1.2 designates the clamping ring of a sealing felt (reference numeral 1.3), and number 3 stands for a glass preform and 4 for the furnace body.

Further mechanical sealing constructions comprise suspended quartz plates used for sealing the feed opening.

It has been suggested to rotate the preform about its central axis during fibre drawing. The rotation provides advantages in terms of controllability of the process, evenness of heating, thickness measurement. However, any ovality of the preform may – in combination with the dragging seals – impair the rotational movement of the preform and, therefore, also the drawing of the fibre as well as the stretching of the preform. Further, particles released from the polymer or graphite materials may contaminate the fibre.

As mentioned above, seals based on mechanical contact with the preform cause contamination of as well as scratches and other defects on the surface of the preform. Instead of elastomer seals, which chemically are highly durable sealing materials, sealing materials that withstand high temperatures must be used. Typically used seals, which are based on graphite felt (see above) or quartz wool, also allow for penetration of oxygen into the furnace and they are subjected to considerable wear. This can be explained by the fact that there is no return flow from the inside of the heating chamber to the outside through the seal that would resist the diffusion generated, or at least it is very difficult to form such a flow in a porous or not completely tight sealing. A narrow slot, the height of which is on the same order as the free travel of a molecule, can be examined in terms of a vacuum, because a vacuum can be defined a space, where the free travel of the molecule is higher than the distance between the walls. In vacuum, the molecule continues its linear travel

between the walls without meeting the oncoming molecule. Thus, an oxygen molecule, for example, that has entered the slot, advances through the slot, once it has gone there. This phenomenon also explains the known fact that molecules are also diffused through a porous wall in the direction of higher pressure. In this light, it is easy to understand that the sealing is either completely tight or it allows a diffusion flow to penetrate, which is difficult to prevent by means of over pressure or other methods. To solve this problem, other means have to be introduced.

In the art, changing the flow of the protective gas has been considered as a solution of the above problem. Thus, US Patents Nos. 4,174,842, 5,970,083 and 5,897,681 and JP Published Patent Application No. JP 60 081039, for example, suggest increasing the gas flow. By this approach, diffusion of oxygen inside the furnace can be decreased, but the particular problem of this solution is that it considerably increases the consumption and expense of inert gas. In fact, when testing non-contacting solutions, extremely high sealing flows have been employed (over 100 standard litre per minute, in the following abbreviated "SLM") and small changes in the structural parts of the whole apparatus have caused surprising failures of seals. In some cases, graphite resistances have deliberately been allowed to be destroyed and they have been changed at a few week intervals. This has been used at least in stretching the preform, and the contaminated preform must have then been cleaned separately.

As will become apparent from the above description of the related art, so far there has not been any proper understanding of the overall heating process of or of the importance of a providing a proper distribution of the flow inside a inductive furnace for glass preforms. Furthermore, the sealing solutions of such furnaces have been separately developed based on individual tests of the various parts. Consequently, even small changes, for example, in the diameter of the preform will give rise to a need for a completely new series of tests before the furnace can be taken into operation.

The controllability in both basic types has been made even more difficult by changes in the geometry of the preforms, such as changes in the thickness, an oval or bowed shape and deflections.

And as explained above, the difficulties mentioned above are aggravated, when the preform is rotated during the process.

### Summary of the Invention

It is an object of the present invention to eliminate the drawbacks of the known technology and to provide a new solution for sealing furnaces used in drawing of optical fibres and stretching of glass preforms and similar operations related to the manufacture of optical fibres.

The invention is based on the idea of maintaining the concentration of gaseous impurities in the heating oven essentially on the same level as the concentration of the same impurities in the inert gas fed into the oven. Further, there is then established a diffusion barrier against the inflow of undesired gaseous components from the ambient air, driven by the forces of diffusion, by generating a barrier flow of inert gas in the inlet opening of the heating oven, said barrier flow having a direction of flow, which is generally opposite to the direction of the diffusion. Thus, in an apparatus according to the present invention, there is formed at least one, preferably as many diffusion barrier zones as there are openings in the furnace chamber. The diffusion barrier will allow the penetration of impurities only in an amount, which will not essentially increase the concentration of impurities in the furnace. Such an increase is preferably less than 10 %, in particular less than 5 %, of the concentration due to the presence of impurities in the protective gas fed into the furnace.

This technical solution is, in particular, carried out by the invention in a method of subjecting a glass preform (work piece) to processing by tensile forces in a furnace to produce a glass product of predetermined shape, wherein at least a part of the glass preform is introduced into the heating oven through an inlet opening, a portion of the glass preform introduced into the heating oven is heated to above the softening point of the glass, the heated portion of the glass preform is subjected to tensile forces in a drawing direction to process the preform into the predetermined shape, the processed portion of the preform having the predetermined shape is drawn from the furnace through an outlet opening, and the softening portion of the preform and at least a part of the processed portion of the preform are flushed in the furnace with inert gas fed into the furnace through a feed opening.

More specifically, the present invention is mainly characterized by what is stated in the characterizing part of claim 1.

The apparatus according to the invention is characterized by what is stated in the characterizing part of claim 17.

The present invention provides considerable advantages. Thus, the solution according to the invention can be used in the manufacture of optical fibre, such as stretching, collapsing, sintering, sleeving of glass blanks, which in the following are also called "preforms", in the processes mentioned above and in various furnaces needed for their combination processes and in a fibre drawing furnace. The invention can be used to provide non-contacting sealing, the consumption of protective gas can be optimised and the number of exact parts minimized by the method described in the invention and, furthermore, it enables simultaneous rotation of the preform. The invention combines and integrates the gas feeding system, the washing or flushing flow of the furnace, the chimney effect, the upper opening (also called the "upper iris", the lower opening (also called the "lower iris", and their physical dimensions.

Thus, the effect of any changes in one part of the whole can be observed and, correspondingly, compensated for in the other parts of the system or by changing the operation or flow distribution or gas feed points of the apparatus. As a result, the number of practical training cycles needed also decreases considerably.

The solution according to the invention provides at least the following advantages:

In combination: non-contacting sealing and use of perform rotation especially in graphite furnaces. The invention will increase the working life of the furnace, in particular or the graphite resistances, and it will reduce the need for regular maintenance of the furnace. In view of the fact that there is less dust and powder (particles) formed by oxidation of the graphite resistances, cleanliness will grow. Importantly, the consumption of protective gas will be decreased compared to the present technical solutions. The flow directions can be changed as desired and the constructional parts of the equipment can be made simple and loosely fitting allowing for a wide variation of the dimensioning.

Furthermore, the invention will provide for transfer of impurities, which are obtained by a selection of the chimney effect, the distribution of flow carried out by means of conductance and the feed point of the protective gas, to an area that is more advantageous for the end product. Below are disclosed various methods of calculating the number of flows, of calculating the chimney effect, of calculating the flow rates and directions in the aggregates. These can be efficiently utilized for the design on new equipment for processing of performs both during stretching and during fibre drawing. The methods allow for dimensioning of the gas feed nozzles.

The present invention discloses methods of defining the velocity of the sealing flow

required by the diffusion for each level of cleanliness and sealing distance, as well as methods for dimensioning the aggregates and flows by using the methods mentioned above.

## 5 Brief Description of the Drawings

In the following, the invention will be examined in detail with the aid of a detailed description and with reference to the appended drawings.

- Figure 1 shows in a schematic fashion the side-view of a process furnace with a preform and its key parts;
- Figure 2 shows a similar side-view of the cross-section of a typical modern solution for sealing the furnace;
- Figure 3 shows the cross-section of a sealing situation implemented according to the invention;
- 15 Figure 4 shows in side-view the advance of a diffusion barrier;
- Figure 5 shows the distribution of a flow of protective gas in a cold furnace or in a horizontal furnace (simple case with one feeding point; c1, c2 and c3 can comprise several subconductances);
- Figure 6 shows a gas flow caused by the chimney effect;
- 20 Figure 7 shows combined duct flows and protective gas flows;
- Figure 8 shows some iris solutions according to the invention;
- Figure 9 shows a preferred embodiment of the invention;
- Figure 10 shows a horizontal section of the embodiment of the previous drawing;
- Figure 11 shows in a schematic fashion the basic flows involved with a chimney effect;
- 25 Figure 12 shows in a schematic fashion the intermediate stage of a process for stretching of a preform
- Figure 13 shows the phase in which the handler of the preform is shoved inside the furnace, and
- Figure 14 shows the end phase of the process, in which sealing occurs between the handler
- 30 and the collar.

## Detailed Description of the Invention

- As discussed above, in the solution according to the invention, any unwanted gaseous
- 35 molecule contents can be kept outside a volume (e.g., a furnace) by using a flow of inert gas to form a diffusion seal. According to the invention, the content of residual is accepted to correspond essentially to (e.g. being slightly in excess of) the level of impurity of the protective gas, for example, and a sealing flow opposite to the diffusion is arranged by

means of the sealing flow, forming a sufficient diffusion seal by means of the sealing distance used. The target concentration of the impurities is typically less than 100 ppm, in particular about 1 to 90 ppm, which can correspond to an excess of 10 %, preferably 5 %, or less of the concentration of impurities in the protective gas.

5

The protective gas used in the present invention can be any inert gas, which is lighter or heavier than air. Typically nitrogen is employed. Argon is more expensive, but it has been found that the consumption of the argon gas is smaller than of nitrogen, which will compensate at least to some extent for the added cost of the gas. Argon has a higher density than air and it will therefore more efficiently revert the chimney flow, as will be explained below.

10

Various technical gases and gas mixtures, such as air, which has been deoxygenized, can also be employed.

15

The invention comprises a furnace assembly having aggregates, which use flows and structural parts that are designed so that the distribution of gases is taken into account in the proportions of conductances, non-contacting sealing by means of a diffusion barrier (sealing condition), possible flow rate and direction of flow over the aggregate conductances, provided by a chimney effect, and combining the above-mentioned flows to define the sealing distances needed. By selecting the actual feed point, it is also possible to control the formation of diffusion barriers in the furnace.

20

As will be explained in more detail below, it is particularly advantageous to design the apparatus in such a way that the opening inlet – in particular the upper opening has a diameter which essentially corresponds to the diameter of the furnace tube (the graphite tube).

25

In practice, and as will be examined in more detail below, it is preferable that in a vertical furnace, the lower iris (lower inlet opening) is wider than the upper iris (a higher conductance). In that case, the upper iris mainly defines the volume of the duct flow (a hatch), and the sealing flow of the lower iris is defined so that it forms a sufficient sealing at the set dimensions. The sealing condition in the upper iris must also be valid, but the duct flow added into the upward component of the protective gas flow is generally so big that the sealing condition is valid for constructions that are sufficiently constricting. For example, the slot of the upper iris should be on a preform of 0.1 to 10 mm, in order for the chimney effect to be suitable. A sealing distance of about 0.5 to 100 mm with reasonable flow levels seems to be enough for the lower iris.

30

35



A first preferred embodiment of the invention is shown in Figure 1, in which the following reference numerals are used:

1. upper iris
- 5 2. lower iris
3. preform having a generally tapered shaped towards one of its end, that end being positioned upwards or downwards,
4. oven chamber
- 5a gas inlet of the protective gas
- 10 5b gas inlet piping of the protective gas
- 5c feed piping of the protective gas
- 6a outlet of the gas flush flow of the oven
- 6b nozzle for the flush gas for feeding gas inside the oven tube
- 7 oven tube

15

In the construction according to the figure, which construction can also be positioned in other directions, such as horizontally, the nozzles of the furnace (or "heating oven"), marked with reference numerals 1, 2, 5 and 7, have been dimensioned such that a diffusion barrier flow is formed in each of them to warrant for sufficient purity. The calculation of the rate of this diffusion barrier flow and the required length of the barrier distances will be discussed below.

20

The actual furnace space is formed by an inner portion of the furnace heating tube 7, wherein the part of the preform, which is to be heated, is positioned. The oven heating tube 25 7 is typically manufactured from graphite and it is heated by means of electric current. This electric current comprises current generated either by induction or by galvanic coupling. The intermediate space between the oven heating tube 7 and the oven chamber 4 is reserved for insulation and, in the case of an induction oven, also for an induction coil. The oven chamber 4 is typically water-cooled.

30

Protective gas is fed into the oven via nozzle 5a, from which it is further conducted via nozzle 5b to the desired location within the oven. The gas can also be fed through the iris construction or it can be fed at several positions 5b, 5c etc., the gas flow being split up at predetermined ratios, through one or more feed nozzles 5a. It is important that the purified 35 protective gas is conducted directly into the oven tube 7 so that any dust released from the insulation would be directed away from the sensitive perform (/or optical fibre) 3. By proper selection of the feed point(s) of the protective gas it becomes possible to influence the direction and the rate of the gas flow within the oven tube and in the various parts of

the oven tube. We have found that by proper adjustment of the rate and flow of the gas, the flow at the centre of the oven tube (the hot zone) can be minimized or even close to zero, if so desired. In the simplified flow model, which is to be presented later, the location of the inlet feed is not considered, but it can easily be added therein.

5

By proper distribution of the gas flows within the furnace it becomes possible to change the gas consumption. Preferably, at least 5 % of the mass flow of the gas is directed downwards, in particular at least 50 %.

- 10 The gas flows can be split up in different subflows outside the furnace, e.g. using various mass flow regulators.

The outflow of gas from the oven is typically accomplished by allowing a part of the gas to leak through the joints in and between the furnace tubes 7 (or through openings made in the  
 15 furnace tubes) into the intermediate space. This flow can be enhanced by partially evacuating the intermediate space via nozzle 6a. This procedure is in use in particular during flushing of the intermediate space before heat-processing in order to remove oxygen and moisture from the oven. During the processing the intermediate space is not flushed. The flushing can be made more effective by creating a distinct flow route, e.g. by a nozzle  
 20 6b made in the oven tube and by fitting the gas outlet nozzle 6a at a position where there are left no pockets which are difficult to flush. Using a construction of this kind, the rate and the distribution of the gas flow within the oven is not dependent on the operation parameters. At the same time, it becomes easier to find the right rates of the gas flows when the various conductances are clearly defined. If desired, it is possible to provide  
 25 suction at the outlet, having a flow rate, which can be adjusted to a desired level by using a mass flow regulator and the gas flow route is determined by vias formed in the construction. The purging can be carried out also with a separate feed nozzle, which is directly connected to the interstitial space.

- 30 By this arrangement it becomes, on one hand, possible to obtain efficient flushing of the intermediate space and, on the other hand, to transport any particles away from the preform. The gas does not either cool the furnace chamber.

It is of particular importance that, with the exception of the above mentioned vias and  
 35 nozzles, the furnace is gas-tight, so as not to allow oxygen to penetrate into the furnace chamber. The flow rate of the protective gas fed into the oven with the mass flow regulator, as well as the flow rate of the flushing gas withdrawn from the intermediate space of the oven, adjusted with the mass flow regulator, then the flow distribution for the upper and

lower irises are exactly known as well as the barrier flows provided thereby.

A furnace provided with properly working diffusion barriers, the oxygen, which deteriorates the graphite parts of the furnaces primarily stems from the carrier gas. It is therefore important to minimize the volume of gas fed into the furnace and to use clean and pure gas for feed through the furnace chamber.

The processed product comprises preferably an optical fibre or a stretched preform. The processed product is preferably continuously, typically during stretching at various drawing speeds, drawn from the furnace.

As will become apparent from the below description of a preferred embodiment, the upper opening can be formed by a graphite tube or a tube made of quartz. The advantage of the latter is that it is inert, whereas the former can be made as a sacrificial substrate which will react with any oxygen before it enters the furnace. The graphite tube also allows for some dragging contact with the surface of the preform.

The sealing is a barrier zone exhibiting essentially laminar flow conditions of the gas. Therefore it is arranged above the feed nozzles of the protective gas. If the nozzles are fitted at the upper opening, a free flow path upwards of about 10 mm and more is preferred. Lengths of about 15 to 1000 mm are possible. By length is meant a length in the direction of the central axis of the furnace tube. The barrier zone is defined by the clearance between the glass preform and the opening of the furnace. The difference between the external diameter of the glass preform and inner diameter of the opening is typically in the range of 0.5 to 15 mm.

#### Dimensioning of the construction according to the present invention

##### Diffusion barrier

I Figure 3, the flowing pattern in the iris is disclosed. A similar barrier flow can be used in other external and internal inlets and outlets according to the invention. The present invention aims at preventing the flow of undesired gas molecules via the inlet (e.g. into the oven). The prerequisite of the dimensioning is that an inflow having a tolerable level of impurities is allowed. Complete purity is not an aim. Such an acceptable level is the concentration of impurities in the inert protective gas (used for producing a barrier flow) or a fraction (e.g. a tenth part) thereof. On the other hand, the effectiveness of the barrier is also influenced by the barrier distance available. The barrier flow can be calculated from

the cross-section of the opening and the volume flow of the barrier flow.

The diffusion barrier conditions can be calculated as follows:

## 5 Equations for gas iris design

### 1) Stationary medium:

Fick's diffusion law in one dimension for concentration  $C(x,t)$ :

10

$$\frac{\partial C(x,t)}{\partial t} = D \frac{\partial^2 C(x,t)}{\partial x^2}$$

15

States that the time derivative of concentration equals the second spatial derivative of the concentration multiplied by a constant  $D$ . Constant  $D$  is defined as the material diffusion constant,  $[D]=[\text{m}^2/\text{s}]$ .

20

Consider a boundary at  $x=0$ , with negative  $x$ -values at left hand side and positive values at right. Assuming constant concentration  $C_s$  at left hand side, and initially ( $t=0$ ) zero concentration at right side, the solution of Fick's diffusion equation would be

$$C(x,t) = C_s, x < 0$$

$$C(x,t) = C_s \left[ 1 - \operatorname{erf} \left( \frac{x}{2\sqrt{Dt}} \right) \right], x \geq 0$$

25 This means that when the time of observation  $t$  goes to infinity ( $\operatorname{erf}(0)=0$ ), concentration reaches  $C_s$  throughout the space.

### 2) Moving medium:

30 In a gas iris the diffusion flow is suppressed by an opposing flow of the medium. Continuing with the above example the medium would flow from right to left in order to counterbalance the diffusion flow.

35

Fick's law for a moving medium has an additional term in the right side of the equation,

$$\frac{\partial C(x,t)}{\partial t} = D \frac{\partial^2 C(x,t)}{\partial x^2} + v \frac{\partial C(x,t)}{\partial x}$$

- where  $v$  is (the magnitude of) the velocity of the medium flowing **from right to left**. The effect of the additional term is to reduce the concentration the more the velocity  $v$  is. Note that the concentration decreases to the right, and the sign of the spatial derivative of  $C(x,t)$  is negative.

Trial function of the form

$$C(x,t) = C_s \left[ 1 - \operatorname{erf} \left( \frac{x + vt}{2\sqrt{Dt}} \right) \right]$$

10

Satisfies the Fick's equation for moving medium.

Another, time independent trial function of the form

$$C(x,t) = C_s \cdot e^{-\left(\frac{v}{D}\right)x}$$

15

satisfies Fick's equation also.

For curiosity, yet another solution exists, namely

20

$$C(x,t) = C_s \cdot e^{+\left(\frac{v}{D}\right)(x+2vt)}$$

However, this one goes to infinity as time  $t$  evolves, so that the solution is excluded as unphysical.

- 25 The general trial function is found by superposing the trial functions above,

$$C(x,t) = C_1(t) \left[ 1 - \operatorname{erf} \left( \frac{x + vt}{2\sqrt{Dt}} \right) \right] + C_2(t) \cdot e^{-\left(\frac{v}{D}\right)x}$$

where

$$C_1(t) + C_2(t) = C_s$$

The time dependence of the solution depends on the error function argument

$$Arg = \frac{x + vt}{2\sqrt{Dt}}$$

5 Time derivative of the argument is

$$\frac{\partial Arg}{\partial t} = \frac{\partial}{\partial t} \left( \frac{x + vt}{2\sqrt{Dt}} \right) = -\frac{x}{4t\sqrt{Dt}} + \frac{v}{4\sqrt{Dt}}$$

which goes zero when time  $t$  satisfies the condition

10

$$v = \frac{x}{t}$$

Thus, if the velocity  $v$  is constant, there will always be a moment in time  $t=t_0$ , that at any point  $x$  the error function argument has a maximum value. When time goes on, the argument will decrease until it finally goes zero with infinite  $t$ .

15

Thus, for infinite  $t$ , the solution is reduced to the time independent term

$$C(x, t = \infty) = C_s e^{-\frac{v}{D}x}$$

20 Considering a gas iris of length  $L$ , the stationary condition states that the concentration behind the gas iris will be

$$C(L, t = \infty) = C_s e^{-\frac{v}{D}L}$$

So that the sealing efficiency of the iris  $E$  is

$$E = \frac{C_s}{C(L, t = \infty)} = e^{+\frac{v}{D}L}$$

25

From the above it is seen that the sealing efficiency rises exponentially with increasing

medium velocity  $v$  or iris length  $L$ .

The iris length  $L$  is obtained from the exponential equation above:

5

$$L = \frac{D}{v} \ln \left( \frac{C_s}{C(L, t = \infty)} \right)$$

(equation 1)

### 6.2.2 Distribution of the protective gas flow

10

In Figure 5a, the distribution of the gas flow ( $F$ ) in the conductances of the upper iris ( $C1$ ), the lower iris ( $C2$ ) and the purge flow of the intermittent space ( $C3$ ) is shown. When the gases flow into the same room, the same feature can be shown as the flow system according to Figure 5b. In a system of this kind, the flow is distributed directly in the ratio of the conductances, which means that, for example, the flow of the upper iris ( $F1$ ) is:

15

$$F1 = F * C1 / (C1 + C2 + C3). \quad (2)$$

The other flows can be calculated in a similar fashion.

20

The conductances can, for their part, be calculated from the following equation:

$$C = K W * H^3 / L, \text{ wherein} \quad (3)$$

25

$C$  stands for conductance

$K$  is a coefficient

$W$  is the width of the slit

$H$  is the height of the slit

$L$  is the length of the slit

30

By considering the geometrical dimensions of the inlets and outlets, the flow velocity in each inlet can readily be calculated and inserted into the equation (1) derived in paragraph 6.2.1. By comparing the barrier length of a physical specimen with the barrier length given by the equation it is easy to determine whether the barrier flow is sufficient or whether it should be altered.

35

From equation (1) it can also be seen that by increasing the length of the barrier slit, the barrier flow needed can be reduced even if it becomes apparent from equation (3) that the conductance increases. By reducing the height of the slit, the flow rate can be increased whereby also a lower flow rate of the barrier gas is needed. This influences conductance to the third potential, equation (3).

When we examine the equation of the gas flow distribution (2) we note that the calculation has been made by iteration because a change in the dimensions of the nozzle (e.g. the iris) will also have an impact on its conductances and thereby on the distribution of the flow over the various conductances. This, on the other hand, changes the flow velocity of the gas fed through the slit and therefore also has a bearing on the required length of the barrier path. One easy way of performing the iterative calculation comprises the use of table calculation.

### 15 Chimney effect

When the furnace is placed in vertical position and when it is warm, a chimney effect based on buoyancy will be generated in the furnace tube. This effect can be calculated as explained in the following (reference is also made to Figure 10):

20

A tube of height  $h$  is kept at temperature  $T_2$ . The surrounding air is at temperature  $T_1$ . Air pressure at the tube exit level (reference level) is  $p_0$ . The pressure at depth  $h$  below the reference level depends linearly on depth  $h$  and gas density  $\rho$  such that outside the tube at depth  $h$ ,

25

$$p_{out} = p_0 + \rho_1 \cdot g \cdot h$$

where  $g = 9.81 \text{ m/s}^2$  is the gravitational acceleration constant. Inside the tube at level  $h$ ,

$$p_{in} = p_0 + \rho_2 \cdot g \cdot h$$

30 The pressure difference at level  $h$ ,  $\Delta p_h$ , is thus

$$\Delta p_h = g \cdot h \cdot (\rho_1 - \rho_2)$$

Density  $\rho$ , temperature  $T$ , and pressure  $p$  are related together for ideal gases by

$$p = \frac{n_{mol}}{V} \cdot R \cdot T = \frac{n_{kpl}}{V} \cdot k \cdot T = \frac{\rho}{M} \cdot k \cdot T = \frac{\rho}{M_{mol}} \cdot R \cdot T$$



For argon gas (Ar), molar weight is  $M_{\text{mol}}(\text{Ar}) = 40 \text{ g/mol}$  and for nitrogen gas,  $M_{\text{mol}}(\text{N}_2) = 28 \text{ g/mol}$ . For air,

5

$M_{\text{mol}}(\text{air}) = 29 \text{ g/mol}$ .  $M$  is the gas molecular weight.

$R$  is the molar gas constant,  $R = 8.314510 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$  ( $= 0.08314510 \text{ bar dm}^3 \text{ mol}^{-1} \cdot \text{K}^{-1}$ ).

$k$  is the Boltzmann constant,  $k = 1.380658 \cdot 10^{-23} \text{ J/K}$ .  $R$  and  $k$  are related together by the

$$k = \frac{R}{N_a}$$

Avogadro constant  $N_a$ , such that

10

$$N_a = 6.0221367 \cdot 10^{23} / \text{mol}.$$

Ideal gas density  $[\text{kg/m}^3]$  is thus

15

$$\rho = \frac{p \cdot M_{\text{mol}}}{R \cdot T} = \frac{p \cdot M}{k \cdot T}$$

If the gas is heated from temperature  $T_1$  to temperature  $T_2$  while keeping the pressure  $p$  constant, its density is reduced accordingly,

20

$$\left. \frac{\rho(T_2)}{\rho(T_1)} \right|_p = \frac{\frac{p \cdot M_{\text{mol}}}{R \cdot T_2}}{\frac{p \cdot M_{\text{mol}}}{R \cdot T_1}} = \frac{T_1}{T_2}$$

$\Leftrightarrow$

$$\Delta \rho = \rho(T_2) - \rho(T_1) = \left( \frac{T_1}{T_2} - 1 \right) \cdot \rho(T_1)$$

The overall pressure difference induced by a heating-cooling cycle at the bottom level of the chimney is obtained by substituting density difference equation to the pressure difference equation above,

25

$$\Delta p = g \cdot h \cdot (\rho(T_2) - \rho(T_1)) = g \cdot h \cdot \left( \frac{T_2}{T_1} - 1 \right) \cdot \rho(T_1)$$

## (Equation 4)

5 The pressure difference can be calculated by inserting the temperature of the furnace and the dimensions thereof into equation 4.

It should be noted from equation 4 that if a gas having a density higher than air is used, then the direction of flow of the protective gas is directed downward. As a result, the gas has to be heated to a temperature higher than about 400 K, at which temperature the chimney flow will turn upwards. This, at the same time means that, at the temperatures mentioned, the mass flow of protective gas needed for reverting the chimney flow is reduced.

When the matter is studied based on the depiction in Figure 6, it can be noted that the pressure difference strives at providing a flow through the conductance of the upper iris (C1 and the conductance of the lower iris (C2). In this example, the conductance of the furnace tube has not been considered because it has been estimated to be of such a magnitude that it bears no influence on the formation of diffusion barriers in the openings. It would, however, be rather straightforward to consider it. The chimney flow can be calculated by using the following equation

$$20 \quad 1/C_{tot} = 1/C1 + 1/C2 \quad (5)$$

for the cumulative effect of serial conductances and

$$25 \quad F_h = C_{tot}(P1^2 - P_o^2) \quad (6)$$

for the chimney flow, wherein

30  $C_{tot}$  is the total conductance and  
 $F_h$  is the chimney flow  
 $P_o$  is the air pressure  
 $P1$  on the sum of the air pressure and the chimney effect

35 Since the chimney effect is directed upwards, the chimney flow has to be added to the flow directed through the upper iris. Correspondingly, it has to be reduced from the flow directed through the lower iris, because it weakens that flow. These features are illustrated in Figure 7.

The rate of the chimney flow is usually significant compared to the barrier flows, which means that it is possible easily to obtain a situation where there is formed a diffusion barrier at the upper iris. The problem to be solved is therefore rather how to create a situation in which the flow rates are sufficiently large to generate a diffusion barrier also at the lower iris.

5

It can be assumed, when looking at the situation more generally, that the required volume flow of protective gas is such that it is sufficient to cover the chimney flow through the upper iris. In addition to that volume, further flow of protective gas should be sufficient also to form a diffusion barrier – when the flow is divided according to equation 2 – also at the lower iris (the flow through the upper iris increases also as shown by equation 2. In such a case, it is preferred to construct the lower iris with a larger clearance between the preform (or optical fibre) and inside of the opening to allow for a greater flow of protective gas to direct the major part, preferably at least 60 volume-%, in particular at least 70 volume-%, of the additional flow downwards. Similarly, it can be deducted from equation 1 that a reduction of the barrier length and the flow slit (increase of flow rate) will reduce the amount of necessary barrier flow. The limit will be reached when the conductance at the lower iris becomes too small (i.e. when a greater part of the flow is directed to the upper iris). Also the slit between the preform and the furnace tube 7 is a conductance, whereby it has to be considered when dimensioning flow rates and volumes. By transferring the feed point from the upper opening towards the lower opening, the ratio between the conductances directed upwards and downwards, respectively, whereby the feed rate for annulling the chimney flow is reduced. The gas consumption is then decreased.

In practice, it can be said that the conductance of the lower iris should be greater than that of the upper iris. On the other hand, the flow needed for creating a diffusion barrier is rather small (only a few SLM) compared to the chimney flow when a barrier length of some 1 to 5 cm is arranged at the lower iris. Then, the clearance at the lower iris can be considerable, which facilitates operation of the equipment. This arrangement becomes particularly advantageous when drawing is made upwards, because it becomes possible to leave ample space for a preform, which is of imperfect shape and, e.g., having bowing and bumps on the surface, whereas the drawn or stretched elongated product, which has a much more exactly defined shape, will pass through the furnace opening at the upper iris, where the clearance should be smaller to allow for a proper diffusion barrier.

As a good rule of thumb, a flow rate comprising the chimney flow + 5 SLM can be mentioned. If necessary, the feed can be increase somewhat to allow for a volume sufficient for flushing of the intermediate space. When a lower opening having an inner diameter of 80 mm and a length of 100 mm, a flow on the above order is sufficient. This flow volume has to be added to the

chimney flow which, depending on the density of the gas, the temperature, the total conductance and the length of the furnace, is on the order of about 5 – 100 SLM.

5 The difference between the external diameter of the preform and the inner diameter of the upper opening is preferably about 1 – 15 mm, and the length of the zone formed above the feed nozzles for the protective gas – providing a zone of laminar gas flow – is about 10 mm to 1000 mm, preferably about 15 – 150 mm.

10 In the above-described situation the upper iris works as a throttle and the flow through it is so large that it is easy to meet the diffusion barrier condition. Similarly, in the lower iris end of the furnace, primarily care has to be taken to see that the diffusion barrier condition is met.

15 The chimney flow can easily be added to the distribution equations of the inert gas for instance by table calculation. It is good to note that changes in the dimensions of the irises also influence the magnitude of the chimney flow. Therefore, a change of one part, influences the whole flow system. It is difficult to see these contrary effects, they always have to be calculated when any changes are to be implemented in the system.

20 Finally, in horizontally placed furnaces, the chimney effect need not be considered. In vertical furnaces it is of significance already at a temperature of 500 °C.

The apparatus according to the invention has been used for the stretching of preforms in the following manner:

25 Figure 12 shows the intermediate stage of the process, Figure 13 shows a phase in which the handler of the preform moves inside the furnace, and Figure 14 shows the end phase of the process in which sealing occurs between the handler and the collar.

30 The apparatus has been designed in such a way that a seal is formed by the slit between the preform and the inner wall of the inlet opening. Since the preform does not contact with the furnace, it can be rotated, if so desired.

35 Towards the end of the process, the handler is moving into the sealing zone, at which stage the seal is formed by the slit between the perimeter of the preform and the inside surface of the inlet opening as well as the slit between the collar and the inside surface of the inlet opening. The diameter of the inlet opening and the perimeter of the collar are dimensioned in such a way that the sealing length of at the upper part of the furnace and the throttling effect do not significantly change at this stage. Rotation of the preform is still possible.

At the end of the process, the collar seals against the inlet opening and the sealing opening is formed by the slit between the collar and the handler. Preferably, this slot is shaped in such a way that the throttling effect of the inlet opening remains constant during the various stages of the process. Rotation of the preform is still possible. If the collar and the inlet opening are not necessarily sealed against each other by using ... or sealing materials, it is possible to leave a slit between them which provides for a sealing flow. Then, the throttling effect of the upper sealing zone is defined by two parallel conductances, viz. the slits between the collar and the handler and between the collar and the inlet opening. In the case examined herein, the chimney effect is much stronger and, at the same time, due care has to be taken that the sealing flow providing a diffusion barrier is strong enough at both ends of the furnace.

When we examine the drawing according to Figure 14, we note that the furnace can be considered to be formed by 5 successive conductances ( $c_1$ ,  $c_2$ ,  $c_3$ ,  $c_4$  and  $c_5$ ) the total effect of which will throttle the chimney flow (for calculating the total effect, formula 5 can be used). Thus, for example in cases in which the slit between the furnace tube and the perform is very narrow, the dominating conductance of the system is formed at this place (the other conductances are smaller, even when taken together, than this conductance), which is the most dominating conductance of the whole arrangement. When this is the case, any variations of the slit of the inlet opening will not influence the magnitude of the furnace flow as dramatically as could be expected by only examining the conductance of the inlet opening. Preferably, the inner diameter of the inlet opening/tube and the inner diameter of the furnace tube should be essentially the same, which allows for minimization of the furnace effect of each inlet opening. In practice, when there is a variation of the sizes of the performs, this is not always attainable outside standard production.

Based on the above, it is easy to understand that by selecting the inlet/feed point of the gas it is possible to influence the amount of gas needed. According to Figure 7, the gas is divided into an upward-directed flow and a downward-directed flow, the respective amounts of which are determined by the ratio between the total conductances of the routes. The upward-directed flow is restricted by the accumulated conductance of the conductances above the feeding point and the downward-directed flow is restricted by the accumulating conductance of the conductances below the feeding point, respectively. The total conductances can be calculated from formula 5. With these total conductances, it is possible to replace the conductances denoted " $c_1$ " and " $c_2$ " in equation 2 (in the case of two outlet,  $c_3$  can be omitted), whereby the flows directed upwards and downwards, respectively, can be calculated. When the position of the feed point is changed from above

the dominating restriction to below it,  $c_1$  is reduced and  $c_2$  is increased. In other words, the part of the flow directed downwards is increased and the amount going upwards is reduced. Thus, by using a smaller flow rate it is possible to obtain a downward-directed flow, which will counteract the downward-directed flow. This feature becomes particularly important

5 when the process is implemented in such a way that the preform is fed from below the furnace and the processed product is withdrawn from the furnace through the upper opening.

In the solution according to the invention, a loose lower opening was employed.

10

### EXAMPLE

In the example, the flow has calculated having the following dimensions:

	Preform diameter	80 mm
15	Preform length	1000 mm
	Stretched preform diameter	42.5 mm
	Handler diameter	45 mm
	Diameter of upper opening	83 mm
	Length of upper opening	100 mm
20	Diameter of lower opening	83 mm
	Length of lower opening	150 mm
	Collar inside diameter	53 mm
	Collar inside length	80 mm
	Collar outside diameter	80 mm
25	Collar outside length	50 mm
	Furnace tube inside diameter	93 mm
	Furnace tube length	400 mm
	Used run parameters:	
30	Inert gas	argon (Ar)
	Temperature	1950 °C

The flow values were calculated at safe size by using formulas 1-6

35 The easiest way is to calculate the chimney effect through the furnace first and then calculate the gas distribution for the used feeding points. The needed diffusion barrier flow for lower iris flow was added to that flow. The sum flow was then used as inert gas flow value.

By using calculated values:

Gas feed under upper opening	30 SLM
Gas feed 150 mm under centerline	15 SLM

5

Generally, feeding a significant part, e.g. about 5 – 100 %, in particular 50 – 100 % (calculated from the fed mass flow), of the gas at or below the centerline of the furnace tube (the point where the temperature is highest in the furnace) has been advantageous in the method and the apparatus according to the invention.

10

The construction worked well and no oxygen damages were noticed.

When the conductances are calculated, it is important to consider what kind of gas actually is employed (e.g. its density) and to apply coefficients for correcting the temperature effects in the equations mentioned above.

15

Within the scope of the present invention, alternative embodiments are also possible. Thus, as shown in Figure 8, it is possible to fit the barrier tube up or inside the furnace or the furnace tube can work as a barrier tube. A combination of these alternatives is also possible. It is further possible to adapt the apparatus to thickness variations by using a plurality of barrier tubes, which are fitted inside each other. The gas feed can take place from an upper inlet, a lower inlet or through a nozzle in the middle of the furnace, or as a combined feed into two or three of these feed points. As discussed above, it is possible to arrange a barrier space inside the furnace to allow for regulation of the flow rates and volumes as a function of the thickness of the preform and the thickness variations thereof.

20

25

Although the above description describes tensional processing, the same principles can be applied to compression processing of glass preforms.

30

**Claims:**

1. A method of subjecting a glass preform to processing by tensile forces in a furnace to produce a glass product of predetermined shape, according to which method

- 5       — at least a part of the glass preform is introduced into the furnace through an inlet opening,
- a portion of the glass preform introduced into the furnace is heated to a temperature above the softening point of the glass,
- the heated portion of the glass preform is subjected to tensile forces in a drawing
- 10       direction to process the preform into the predetermined shape,
- the portion of the preform which has been processed into the predetermined shape is drawn from the furnace through an outlet opening, and
- the heated portion of the preform and at least a part of the processed portion of the
- 15       preform are flushed in the furnace with inert gas which is being fed into the furnace,

characterized by

- maintaining the concentration of gaseous impurities in the furnace essentially on the same level as the concentration of the same impurities in the inert gas fed into the oven,
- 20       — establishing a diffusion barrier against the inflow of undesired gaseous components from the ambient air, driven by the forces of diffusion, by generating a barrier flow of inert gas in at least one opening selected from said inlet opening and said outlet opening of the furnace, said barrier flow having a direction of flow, which is generally opposite to the direction of the diffusion.

25

2. The method according to claim 1, wherein the furnace comprises an elongated furnace chamber having a vertical central axis, said diffusion barrier being established in the inlet opening, which is located in the upper end of the elongated furnace chamber.

30 3. The method according to claim 1 or 2, wherein a diffusion barrier is established in the inlet opening of the glass preform, in the inlet opening of the inert gas feed and in the outlet opening of the processed preform.

35 4. The method according to claim 2, wherein the gas flow through the inlet opening of the glass preform corresponds to the equation (2)

$$F_1 = F \cdot C_1 / (C_1 + C_2).$$

(2)



wherein

F1 stands for the gas flow through the inlet opening,

F stands for the total gas flow,

C1 stands for the conductance of the inlet opening and

5 C2 stands for the conductance of the outlet opening

5. The method according to claim 4, wherein the each of the conductances C1 and C2 is be calculated from the equation (3)

10  $C=K W^3/H/L,$  (3)

wherein

C stands for conductance,

K is a constant at low pressure differences,

15 W is the width of the opening,

H is the height of the opening, and

L is the length of the opening

6. The method according to any of claims 1 to 5, wherein the flow of inert gas through the opening is at least equal to the flow of gas caused by the chimney effect through the inlet opening.

7. The method according to claim 6, wherein the flow or inert gas into the heating oven is sufficient still to form, based on the gas distribution according to equation (2), a diffusion barrier at the outlet opening of the processed preform.

8. The method according to claim 7, wherein the outlet opening will allow for more free flow of gas than the inlet opening to direct most of the inert gas flow fed into the oven through the outlet opening.

9. The method according to any of claims 3 to 8, wherein the conductance of the outlet opening is greater than the conductance of the inlet opening.

10. The method according to any of the preceding claims, wherein the inert gas fed into the heaving oven is equal to or greater than the flow of gas caused by the chimney effect + 1 SLM, in particular chimney effect + 5 SLM.

11. The method according to any of the preceding claims, wherein the glass preform is

subjected to tensile drawing in order to stretch the preform into a shape suitable for post-processing like drawing of optical fibres.

12. The method according to any of claims 1 to 10, wherein the glass preform is subjected to drawing of optical fibre.

13. The method according to claim 12, wherein the clearance between the exterior diameter of the glass preform and the inlet opening diameter is 0.1 – 10 mm for an 80 mm preform.

14. The method according to claim 12, wherein there is a barrier flow along a barrier distance of 0.5 to 100 mm.

15. The method according to any of claims 1 to 14, wherein the furnace comprises a graphite induction furnace.

16. The method according to any of the preceding claims, comprising rotating the glass preform about its central axis during heat-processing in the furnace.

17. An apparatus for heating of glass performs which are processed by tensile forces into a glass product of predetermined shape, comprising

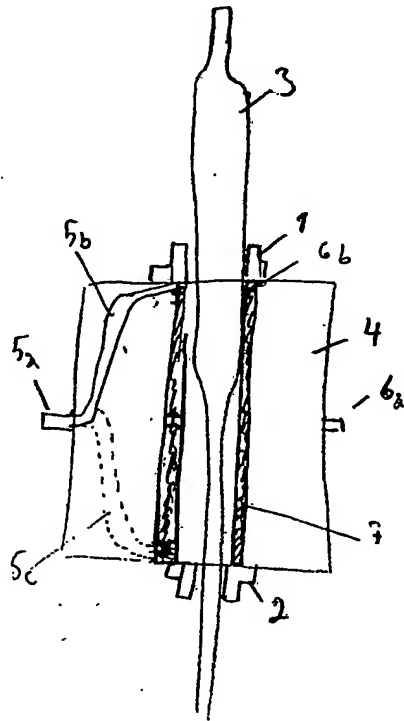
- a furnace body having a jacket defining an elongated furnace chamber with an at least essentially circular cross-section perpendicular to the central axis of the chamber,
- a first opening at one end of the chamber for receiving one end of a glass preform, which is to be processed,
- a second opening at an opposite end of the chamber for withdrawal of the processed glass product,
- graphite heating resistances mounted to the furnace chamber to provide for induction heating of the glass preform in the furnace, and
- feed nozzles connected to at least the first opening of the chamber for introducing protective gas into the furnace chamber,

characterized by

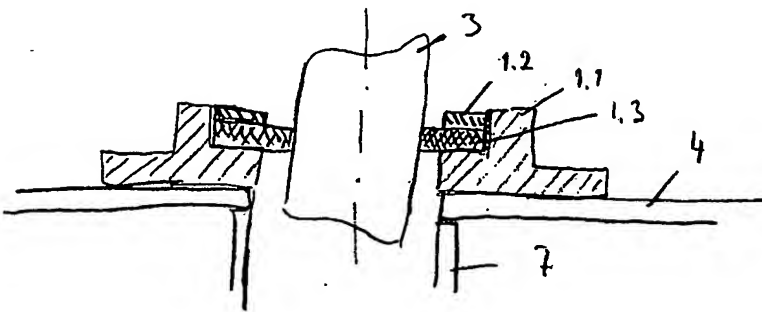
- a first diffusion barrier zone at the first opening for preventing inflow of undesired gaseous components from the ambient air, driven by the forces of diffusion, into the furnace chamber during heating of the glass preform.

18. The apparatus according to claim 17, wherein there is a second diffusion barrier zone at the second opening of the furnace chamber.

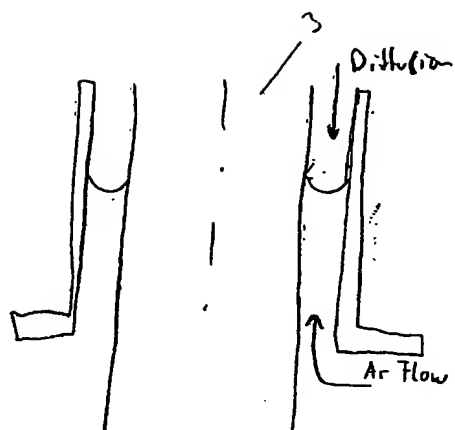
19. The apparatus according to claim 17 or 18, wherein a nozzle for feed of protective gas is connected to both the first and the second openings and, optionally, also to an opening formed in the jacket of the furnace chamber at a point between the first and the second openings.
20. The apparatus according to any of claims 17 to 19, wherein the apparatus is adapted for heating of a glass preform subjected to drawing of optical fibre.
21. The apparatus according to claim 20, wherein the clearing between the exterior diameter of the glass preform and the inlet opening diameter is 0.1 – 10 mm for an 80 mm preform.
22. The apparatus according to claim 21, wherein the each barrier zone comprises a length of the furnace chamber amounting to 0.5 to 100 mm, along which a barrier flow of protective gas can be arranged.
23. The apparatus according to any of claims 17 to 22, wherein the barrier zone comprises a zone of essentially laminar gas flow.
24. The apparatus according to claim 23, wherein the barrier zone is formed above the feed nozzles of the protective gas.
25. The apparatus according to any of claims 17 to 24, wherein the barrier zone is defined by the clearance between a glass preform and the opening of the furnace.
26. The apparatus according to claim 25, wherein the difference between the external diameter of the glass preform and inner diameter of the opening is in the range of 0.5 to 15 mm.
27. The apparatus according to any of claims 23 to 26, wherein the barrier zone has a length parallel to the central axis of the furnace tube amounting to about 10 to 1000 mm, preferably about 15 to 150 mm.



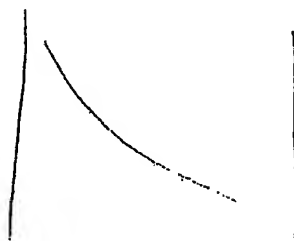
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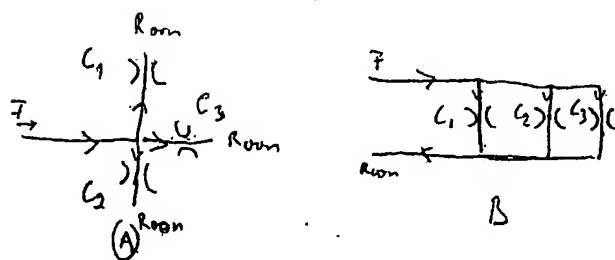
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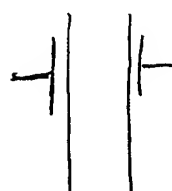
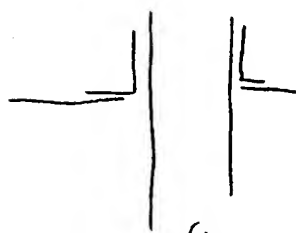
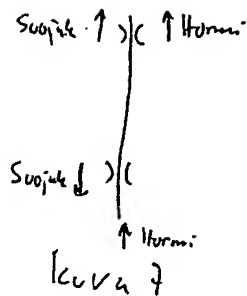
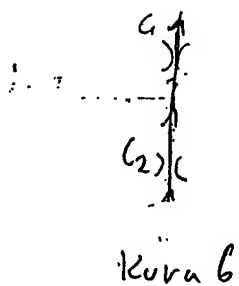
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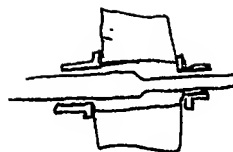
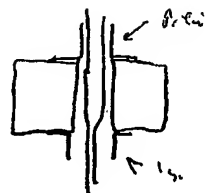
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kuva 8



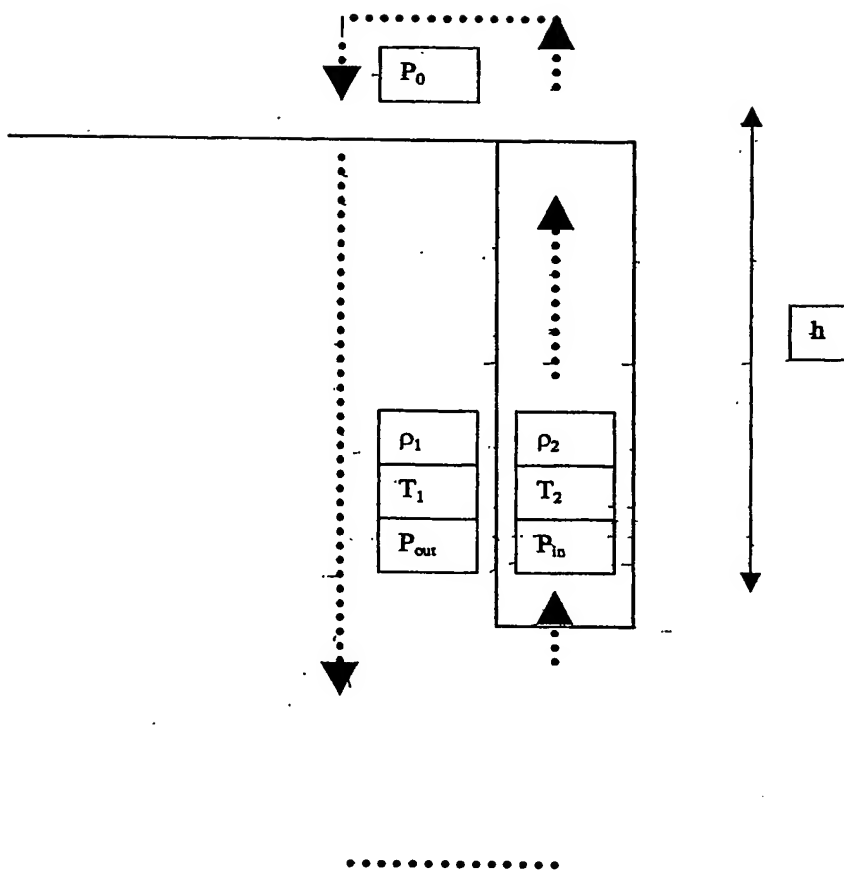


Fig. 11

Fig. 12

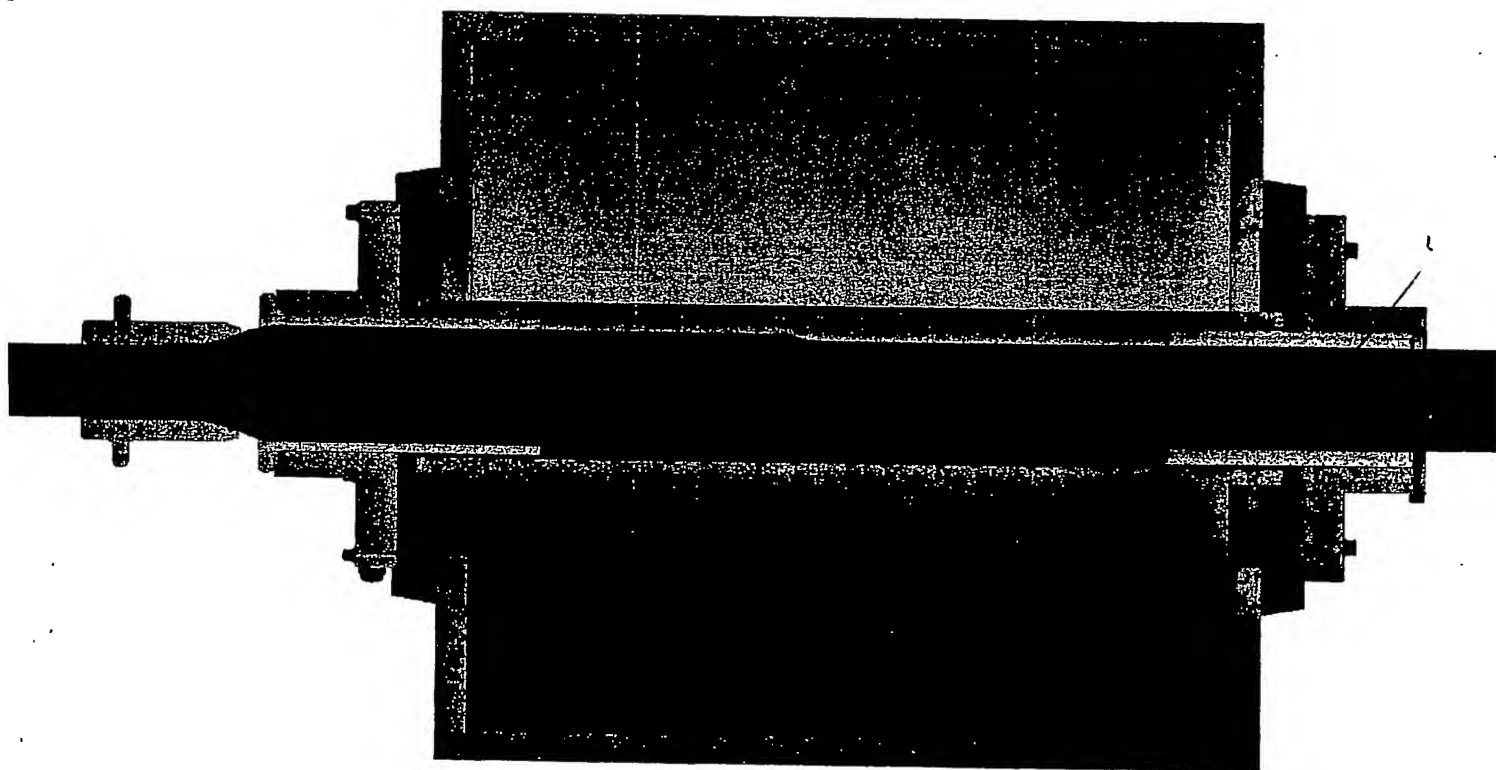
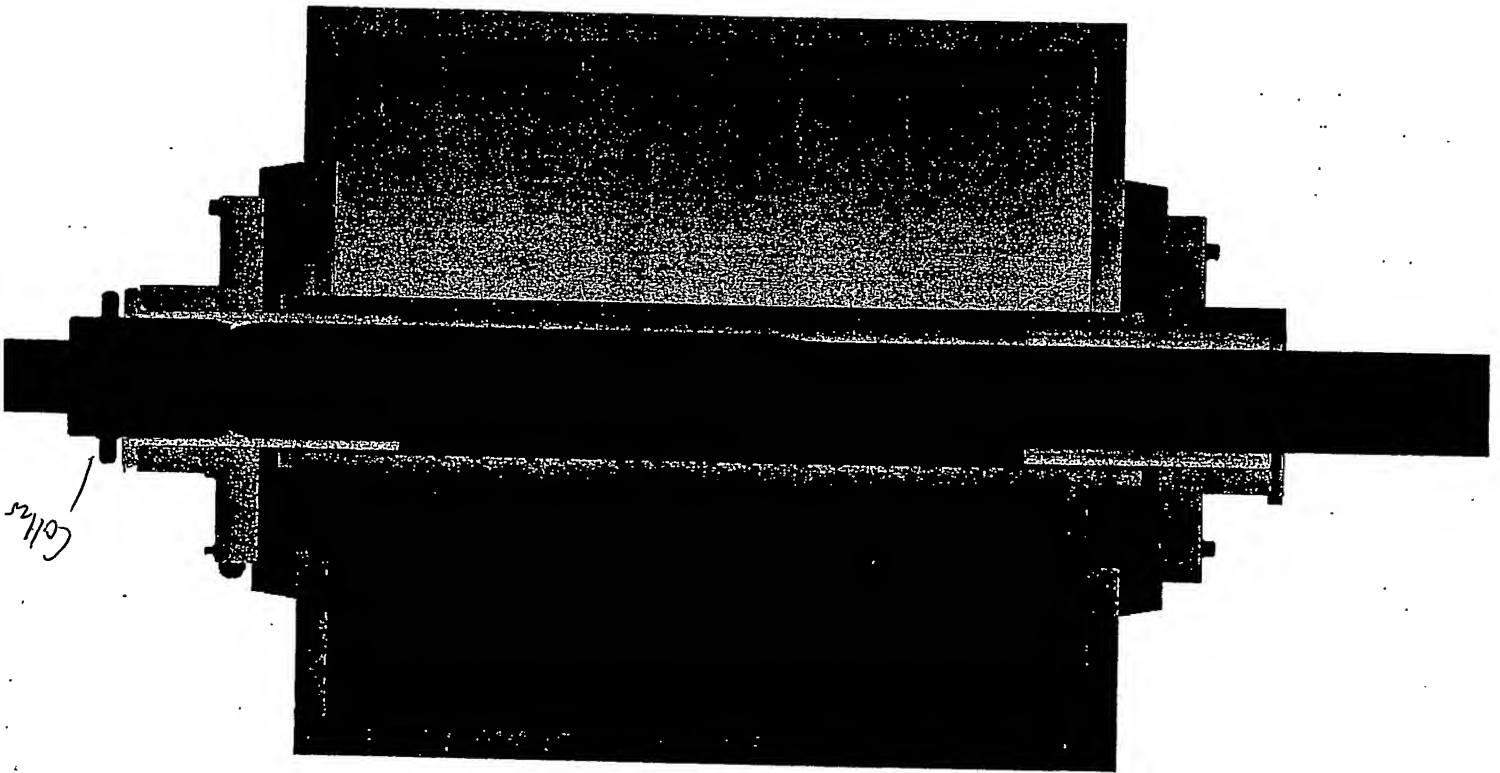




Fig. 13



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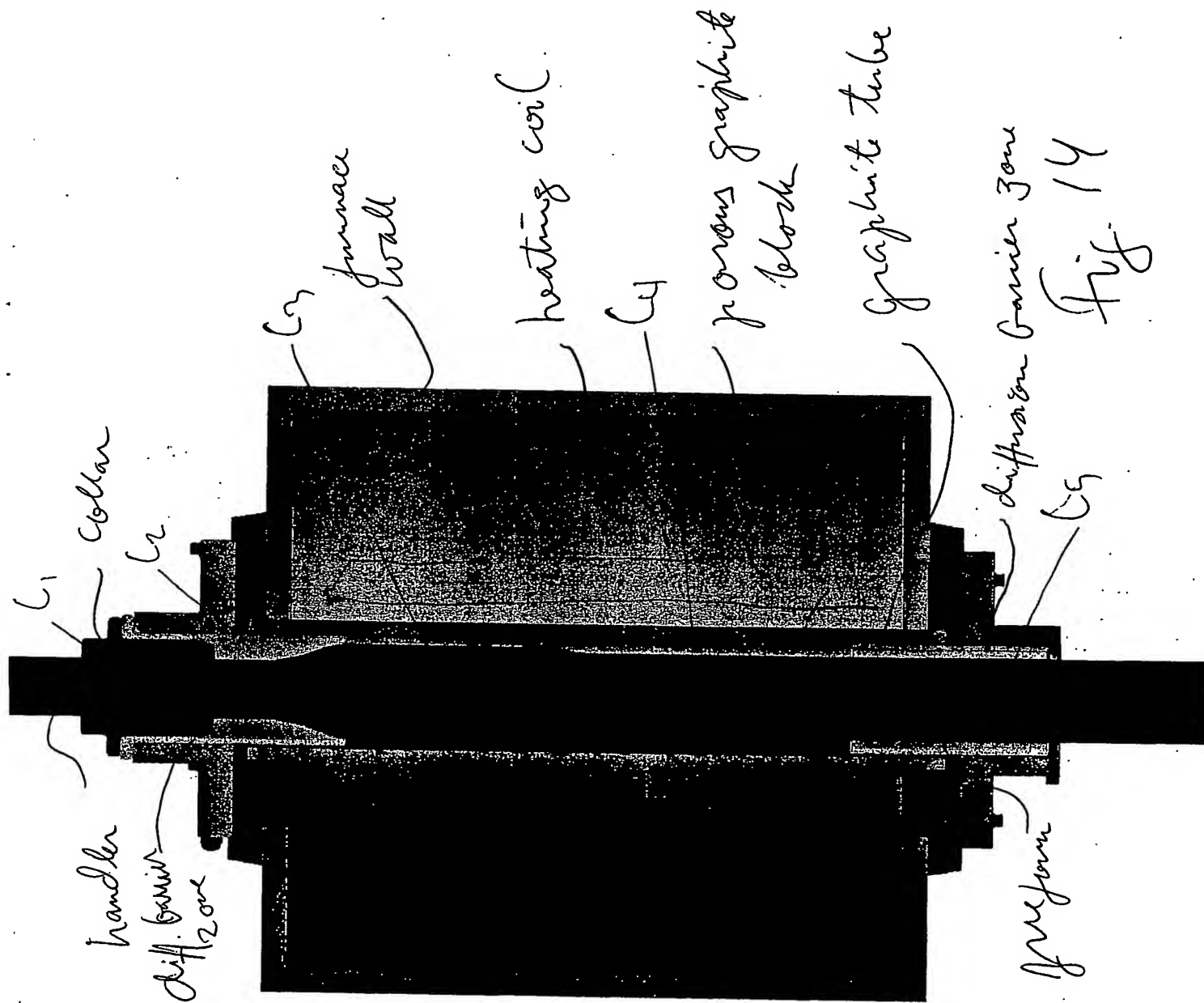


Fig. 14

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